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<p>(21) International Application Number: PCT/US98/24476</p> <p>(22) International Filing Date: 16 November 1998 (16.11.98)</p> <p>(30) Priority Data: 08/971,514 17 November 1997 (17.11.97) US</p> <p>(71) Applicant: CONTINUUM ENVIRONMENTAL, INC. [US/US]; 128 Lockport Street, Youngstown, NY 14174 (US).</p> <p>(72) Inventor: CONAWAY, Lawrence, M.; 321 3rd Street, Youngstown, NY 14174 (US).</p> <p>(74) Agent: SLIFKIN, Neal, L.; Harris Beach & Wilcox, LLP, 130 East Main Street, Rochester, NY 14604-1687 (US).</p>		<p>(81) Designated States: AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, GH, GM, HR, HU, ID, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, UZ, VN, YU, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).</p> <p>Published <i>With international search report.</i> <i>With amended claims.</i></p>	
<p>(54) Title: SYSTEM FOR PROCESSING OIL REFINERY WASTE</p> <pre> graph TD 12[WASTE FEED] --> 14[SCREEN] 14 --> 18[CONDITIONING VESSEL] 18 --> 22[FIRST CENTRIFUGE] 22 -- FIRST EFFLUENT --> 24[TO REFINERY] 22 -- FIRST CAKE --> 20[STEAM GENERATOR] 20 --> 28[Hot Water] 28 --> 26[REACTOR TANK] 26 --> 26a[AUXILIARY REACTOR TANK] 26a --> 32[SECOND CENTRIFUGE] 32 -- SECOND EFFLUENT --> 24 32 -- SECOND CAKE --> 36[DEWATERING] 36 --> 34[SOLIDS DISPOSAL] 20 --> 26 28 --> 26 26 --> 26a </pre>			
<p>(57) Abstract</p> <p>Refinery waste feedstock is screened in a screen (14) to remove large particles and is diluted to less than 5 % solids weight percent to form a first slurry which is agitated and heated to 180 degrees Fahrenheit in a conditioning vessel (18). The conditioned first slurry is passed through a first centrifuge (22) which separates the conditioned first slurry into a first liquid effluent and a first residual cake. The first residual cake is diluted with hot water and treated with hydrogen peroxide in a reactor tank (26) to form a second slurry and lyse and/or liberate petroleum compounds and oxidize toxic polycyclic aromatic hydrocarbons to non-toxic derivatives. The second slurry is passed through a centrifuge (32), yielding a second liquid effluent and a residual cake containing about 0.5 % or less petroleum and about 70 % solids, which may be landfilled directly or further dewatered as needed.</p>			

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SYSTEM FOR PROCESSING OIL REFINERY WASTE

5 The present application is a Continuation-In-Part of my pending application, Serial Number 08/807,643 filed February 27, 1997.

Description

10 The present invention relates to methods and apparatus for treatment of sludges and contaminated solids to recover hydrocarbons therefrom, and more particularly to a system (methods and apparatus) for processing of K-wastes from oil-contaminated sites such as refinery storage tanks, distillation 15 columns, and soils to recover hydrocarbons therefrom and to render the residues suitable for environmentally-acceptable disposal.

20 Residual sludges are inherent in the storage and refining of petroleum. Depending upon the source of the crude oil, the petroleum feedstock delivered to a refinery may contain various 25 non-refinable contaminants which typically may include silt, salt, sulfur, metals, and ash. The crude oil itself inherently contains small quantities of fine solids which can settle in the bottom of storage tanks and are so tightly bound to hydrocarbons as to resist conventional separation processes such as filtration and centrifugation. When petroleum feedstocks are refined in fractionation columns, various high molecular weight organic compounds and various inert components are condensed or trapped in the still bottoms.

30 The storage and distilling residues which are environmentally unsuitable for disposal are said to be "K-listed" by the US Environmental Protection Agency and are known in the

refining art as "K-waste." As used herein, the term "refinery waste" means collectively the residuals of all petroleum acquisition, transporting, storing, and refining operations, and includes but is not limited to sludges, bottoms, waxes, oils, 5 greases, and contaminated soils. The USEPA has imposed restrictions on disposal of these wastes, mandating that such waste must be treated to meet specific "Best Demonstrated Available Treatment" (BDAT) standards before the contaminated substrate may be disposed of, typically by landfill.

10 Over the past few years, disposal regulations have become more stringent and cost of processing petroleum-contaminated soils and sludges has escalated. Both of these trends may be expected to continue in the future. Current technologies for dealing with refinery waste are very expensive to implement and 15 frequently are inadequate to meet current and future regulations.

20 "Landfarming," wherein natural degradation of petroleum waste is accomplished via biological reduction in impoundments, is slow, expensive, consumptive of space, requires elaborate mechanisms of control, and can fail ultimately to meet the requirements for reduction of high molecular weight hydrocarbons.

25 Processes to reduce the volume of material to be landfilled can remove up to 80-85% of the volume of raw waste. Various centrifugal separators and/or filtration systems can be used to separate out the dirt fraction from the liquid components, including water and oils for return to the refinery. However, achieving good filter separation typically requires the use of diatomaceous earth which produces a fluffy cake having a high petroleum content; and further, the dirt fraction of the filter cake still contains a high level of bound petroleum.

30 Where centrifugal decanter centrifuges are employed for separation and volume reduction, polymers typically are added

ahead of the decanter to flocculate solids for easier settling. In some instances, solvents or "cutter stock" are added to reduce the viscosity of heavier fractions to improve separation.

5 However, the thrust of this process generally is to return oil to the refinery within a given specification for bottom sediment and water (BS&W), and little regard is placed on the cleanup of the solid or cake fraction destined for disposal. Thus, landfill disposal of the solid residue is wasteful of its refinable petroleum content.

10 To remove further water and petroleum from the decanter cake, some treatment processes include an additional thermal desorption or outright incineration of the decanter cake. However, both processes are additionally expensive in being high in demand for maintenance, labor, and energy to meet current BDAT 15 standards imposed under the Federal Resource Conservation and Recovery Act (RCRA), and incineration is wasteful and precludes further petroleum recovery from the cake. Further, adding either of these processes to the mechanical separation process is a, add-on approach and does not address the up-front problem of 20 petroleum fractions tightly bound to finely-divided particles of silt and soil, or the potential commercial benefit of recovering those fractions.

25 Thus there is a need for a re-engineered complete process which is cognizant of the fundamental need to free petroleum fractions from silts and soils and which can provide a highly efficient and relatively inexpensive method for treating refinery wastes, including K-listed wastes, to separate virtually all the refinable petroleum fraction from the solids therein and to provide a residual solid fraction for disposal which can be 30 delisted under RCRA guidelines.

It is a principal object of the invention to provide an

improved process for treating refinery wastes which provides a residual solid fraction for disposal which can be delisted under RCRA guidelines.

It is a further object of the invention to provide an improved process for treating refinery wastes which can readily separate petroleum from silts and soils and thereby return a high percentage of the refinable petroleum fraction therein to the refinery.

It is a still further object of the invention to provide an improved process for treating refinery wastes which is less expensive to operate on a per-unit of waste basis than known treatment processes.

It is a still further object of the invention to provide an improved process for treating refinery wastes which is easily retrofittable to existing facilities.

Briefly described, in a totally-engineered refinery waste treatment system embodying the invention, waste feedstock to be treated is screened to remove large particles and is diluted to a solids weight percent of less than 5% to form a waste slurry. In a feed/mix tank, the slurry is agitated and heated to 180°F or higher for a time sufficient to melt waxy petroleum solids, reduce the viscosity of the batch, reduce the density of petroleum fractions within the batch, and begin to break surface adhesion of petroleum to inert surfaces. The thus-conditioned slurry is treated by a first disc/bowl centrifuge. Greater than 80% of the waste volume is separated by the centrifuge, and the liquid effluent which contains most of the petroleum fractions from the original waste may be returned to the refinery for processing. In a reactor tank, the residual cake, which may contain about 5% or less of oil and grease, is diluted with hot water to form a second slurry and is treated with hydrogen

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peroxide in amount and for a time sufficient to lyse and liberate the petroleum fraction bound to fines in the waste and to oxidize toxic polycyclic aromatic hydrocarbons to non-toxic derivatives.

The second slurry is treated by a second disc/bowl centrifuge.

5 The liquid effluent is combined with the stream from the first centrifuge, and the residual cake which may contain about 0.5% or less of petroleum fractions and about 70% solids may be landfilled directly or further dewatered as needed to meet disposal requirements.

10 The foregoing and other objects, features, and advantages of the invention, as well as presently preferred embodiments thereof, will become more apparent from a reading of the following description in connection with the accompanying drawing of which FIG. 1 is a schematic diagram of a system for 15 processing refinery waste in accordance with the invention.

The objectives of the subject process are:

20 a) to accommodate a refinery waste stream, including K-listed wastes, resulting, for example, from storage tank cleanings, storm runoff accumulations, slop tank washouts, still bottom residues, refinery soils, and the like, having a wide range of compositions and including varying percentages of light fractions, heavy fractions, asphaltines, carbon, silt, sand, salts, sulfur and sulfur compounds, and polycyclic aromatic hydrocarbons (PAH's);

25 b) to liberate and recover virtually all of the petroleum content of the waste stream and to return it to the refinery for processing into saleable products;

30 c) to carry out such liberation and recovery without resort to flocculants or filter aids such as diatomaceous earth or polymers;

d) to convert toxic substances in the waste stream into non-

toxic derivatives;

5 e) to yield a residual solid which is substantially free of hydrocarbon residues (0.5% or less) and which may be delistable and is suitable for disposal in accordance with government regulations; and

 f) to meet all of the above objectives efficiently and economically.

10 Referring to FIG. 1, there is shown a refinery waste treatment system 10 embodying the invention. Since waste volumes to be treated can be relatively large, on the order of tens of thousands of barrels or more at a time, it is generally preferable to configure system 10 for continuous throughput, although semi-continuous and batch systems are within the scope of the invention.

15 Waste feedstock 12 to be treated is diluted with water to a solids weight percent of less than 5% to form a waste slurry and then is passed through screen 14 to remove large particles, preferably a No. 10 sieve which removes particles larger than 2mm in diameter. The removed particles are discarded as debris 16.

20 In a feed conditioning vessel 18, the slurry is agitated and heated to 180°F or higher for a time sufficient to melt waxy petroleum solids, reduce the viscosity of the batch, reduce the density of petroleum fractions within the batch, and begin to break surface adhesion of petroleum to fine particles in the waste. A suitable length of conditioning will vary with the 25 type, volume, and mix of wastes presented to the process.

30 Preferably, vessel 18 is provided with a narrow neck to minimize the surface area of the slurry and thereby to minimize the evolution of hydrocarbon gases therefrom. Vessel 18 is provided with either a controlled inert atmosphere or a controlled air flow in the headspace in the vessel to prevent the

concentration of such gases from exceeding the lower explosive limit. Combustible evolved gases may be passed to the atmosphere or may be used advantageously as described hereinbelow.

5 The slurry in vessel 18 may be heated by steam jacket or, preferably, by direct injection of steam into the waste as supplied from a conventional steam generator (boiler) 20.

10 After conditioning is substantially complete, the conditioned slurry is treated by a first centrifuge 22, preferably a high-efficiency disc/bowl centrifuge as is known in the pharmaceutical manufacturing arts. Horizontal decanter centrifuges are known to be used in the refinery waste processing art for volume reduction, and they can achieve reasonably good quality of the liquid separation fraction. However, they have relatively low separating efficiencies and typically require the 15 addition of flocculants or coagulating aids to the slurry to achieve adequate separation of solids. The resulting polymer floc can have a spongy structure which reduces cake density and retains unacceptably high levels of water and oils within the cake. It has been found that use of a disc/bowl centrifuge at 20 this stage obviates the requirement for flocculation of the slurry and yields a much denser cake having relatively low liquid content, which is a stated objective of the invention. Centrifuge 22 may be of batch, semi-continuous, or continuous discharge design.

25 Greater than 80% of the waste volume is separated by the centrifuge 22, and the liquid effluent which contains most of the petroleum fractions from the original waste may be returned 24 to the refinery for processing.

30 The residual cake typically is not yet suitable for landfill disposal and requires further processing or conversion. In a reactor tank 26, the cake, which may contain about 5% oil and

grease, is agitated and diluted with hot water 28, preferably at about 180°F or higher to form a second slurry and is treated with hydrogen peroxide 30 in an amount and for a time sufficient to lyse and/or liberate the residual petroleum still bound to fines 5 in the cake. Long-chain hydrocarbons are converted to shorter-chain molecules forming a lighter petroleum fraction suitable for re-submission to the refinery. This treatment step also oxidizes toxic polycyclic aromatic hydrocarbons to non-toxic derivatives, for example, naphthalene and anthracene may be oxidized to 10 naphthaquinone and anthraquinone, respectively. Some volatile hydrocarbon release is generated during this conversion stage requiring controlled venting of tank 26. Advantageously, these gaseous hydrocarbons may be captured and burned to fuel steam generator 20 along with similar volatiles from feed digestion 15 vessel 18, or they may be passed to the atmosphere. Addition of water and hydrogen peroxide may be on a batch, semi-continuous, or continuous feed basis. A plurality of reactor tanks 26a like reactor tank 26 may be employed in parallel with tank 26 to increase the throughput capacity of the overall waste processing 20 system.

Upon completion of the reactor stage in tank 26, the second slurry is fed to a second centrifuge 32, again preferably a disc/bowl centrifuge, to remove light petroleum fractions generated during the reactor stage. The liquid effluent may be 25 combined with the stream from the first centrifuge 22, and the residual cake which may contain about 0.5% or less petroleum fractions and about 70% solids may be disposed of directly 34 or further dewatered 36 and/or dried by known means as needed to meet disposal requirements.

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Example:

A crude oil storage tank has a bottom sludge buildup consisting of 50% inert solids and 50% petroleum compounds and amounting to 20,000 barrels. Pressure water blasting and vacuum truck removal is selected to clean the tank for inspection and 5 deinventorying of waste. Tank cleaning requires 80,000 barrels of water, resulting in a total of 100,000 barrels of liquid petroleum waste. In gravimetric terms, the waste comprises 1890 tons (10.66%) of inert solids, 1890 tons (10.66%) of petroleum compounds, and 13,944 tons (78.67%) of wash water.

10 If containment capacity is available, the waste is allowed to settle and stratify and about 50% of the water volume is decanted and discarded. The remaining 50% of the waste is treated in a continuous processing system in accordance with the system described hereinabove.

15 Processing cost of 100,000 barrels at, for example, \$4.20 per barrel is \$420,000. Disposal cost of 1890 tons of inert solids at, for example, \$210 per ton is \$400,000. Total handling costs are \$820,000.

20 Comparing the cost of treatment in accordance with the invention to expected costs incurable using known technologies for the same waste, direct offsite incineration in a commercial liquid phase incinerator is estimated to cost at least \$3 million and could be as high as \$5 million depending upon difficulty in handling a particular sludge in a liquid injection incinerator; 25 volume reduction and drying followed by offsite solids phase commercial incineration is estimated to cost at least \$2.5 million; volume reduction with thermal desorption of the residual cake is estimated to cost at least \$2.0 million; and volume reduction with BTU enhancement (addition of a sacrificial petroleum fraction) to improve burning is estimated to cost at 30 least \$2.3 million.

From the foregoing description it will be apparent that there has been provided an improved system (method and apparatus) for processing refinery wastes to recover residual petroleum therein and to prepare residual solids for environmentally-
5 acceptable disposal, wherein refinery wastes are conditioned in hot water; subjected to first centrifugation in a first disc/bowl centrifuge to separate a refinable liquid from a first cake; subjected to hydrogen peroxide conversion to lyse and/or liberate petroleum compounds from inert solids and to convert toxic
10 compounds into non-toxic derivatives; and subjected to second centrifugation in a second disc/bowl centrifuge to separate the liberated petroleum compounds for refining and to yield a semi-dry cake suitable for direct disposal or further dewatering.
Variations and modifications of the herein described system, in
15 accordance with the invention, will undoubtedly suggest themselves to those skilled in this art. Accordingly, the foregoing description should be taken as illustrative and not in a limiting sense.

What is claimed is:

1. A method for treating an aqueous slurry of refinery wastes to provide effluent from which petroleum products may be recovered and a cake which is substantially free of hydrocarbon residues, comprising the steps of:

a) heating said waste slurry to a temperature of about 180°F or higher, and maintaining said slurry at said temperature for a period of time sufficient to condition said slurry, including melting any entrained petroleum solids, reducing the apparent viscosity of the slurry, and reducing the density of petroleum fractions in said slurry;

b) passing said hot digested slurry through a first centrifuge to separate a first liquid effluent containing liquid petroleum fractions from a first cake containing bound petroleum residues;

c) dispersing said first cake in water to form a second slurry;

d) treating said second slurry by adding an amount of hydrogen peroxide thereto to lyse and liberate said bound petroleum residues from inert solids contained in said first cake; and

e) passing said second slurry through a second centrifuge to separate a second liquid effluent containing petroleum fractions from a second cake, said second cake containing said inert solids and being substantially free of hydrocarbon residues.

2. A method in accordance with Claim 1 further comprising the step of adjusting the weight of solids in said waste to about 5 percent or less prior to said heating step.

3. A method in accordance with Claim 1 further comprising the step of passing said aqueous slurry through a screen to remove large particles therefrom prior to said heating step.

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4. A method in accordance with Claim 1 further comprising the step of directing said first and second liquid effluents to a refinery.

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5. A method in accordance with Claim 1 further comprising the step of at least partially dewatering said second cake.

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6. A method in accordance with Claim 1 wherein said treating step includes oxidizing polycyclic aromatic hydrocarbons in said second slurry.

7. A method in accordance with Claim 1 wherein said heating step includes injection of steam into said slurry.

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8. A method in accordance with Claim 1 wherein at least one of said first and second centrifuges is a disc/bowl centrifuge.

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9. A method in accordance with Claim 1 wherein said waste slurry contains K-listed waste.

10. A method in accordance with Claim 1 wherein said water in said dispersing step is heated.

30

11. A system for processing oil refinery waste to

provide liquid effluent from which petroleum products may be recovered and a cake which is substantially free of hydrocarbon residues, comprising:

5 a) a conditioning vessel for receiving, tempering, and otherwise thermally conditioning a slurry of said waste;

10 b) a first centrifuge in communication with said conditioning vessel for receiving said conditioned slurry therefrom and separating said first slurry into a first liquid effluent and a first cake, said first effluent being refinable into petroleum products;

c) a reactor vessel for receiving said first cake;

15 d) means for dispensing hydrogen peroxide and water into said reactor vessel to form a second slurry with said first cake and to lyse and liberate bound petroleum residues from inert solids contained in said first cake;

20 e) a second centrifuge in communication with said reactor vessel for receiving said second slurry therefrom and separating said second slurry into a second liquid effluent and a second cake, said second effluent being refinable into petroleum products and said second cake being substantially free of petroleum residues.

25 12. A system in accordance with Claim 11 wherein at least one of said first and second centrifuges is a disc/bowl centrifuge.

13. A system in accordance with Claim 11 wherein said conditioning vessel is provided with steam for said tempering of said slurry.

30 14. A system in accordance with Claim 11 further

comprising at least one additional reactor vessel arranged for parallel flow with said first reactor vessel.

15. A system in accordance with Claim 11 further comprising means for maintaining non-explosive atmospheres within 5 said conditioning and reactor vessels.

16. A system in accordance with Claim 11 further comprising a screen for filtering large particles from said waste 10 before introducing said waste to said conditioning vessel.

17. A system in accordance with Claim 11 further comprising means for diluting said waste with water to a weight percentage of about 5 percent or less.

15
18. A system in accordance with Claim 17 further comprising means for capturing volatile hydrocarbons escaping from said slurries and combusting said hydrocarbons to heat said water.

20
19. A system in accordance with Claim 11 further comprising means for dewatering said second cake.

AMENDED CLAIMS

[received by the International Bureau on 26 March 1999 (26.03.99);
original claims 1,5 and 9 amended; remaining claims unchanged (4 pages)]

1. A method for treating an aqueous slurry of refinery wastes to provide effluent from which petroleum products may be recovered and a cake which is substantially free of hydrocarbon residues, comprising the steps of:

- a) heating said waste slurry to a temperature of at least about 180°F to form a hot sludge;
- b) maintaining said slurry at said temperature for a period of time sufficient to digest said hot sludge, said digestion including melting any entrained petroleum solids, reducing the apparent viscosity of the slurry, and reducing the density of petroleum fractions in said slurry;
- c) passing said hot digested slurry through a first centrifuge to separate a first liquid effluent containing liquid petroleum fractions from a first cake containing bound petroleum residues;
- d) dispersing said first cake in water to form a second slurry;
- e) treating said second slurry by adding an amount of hydrogen peroxide thereto to lyse and liberate said bound petroleum residues from inert solids contained in said first cake; and
- f) passing said second slurry through a second centrifuge to separate a second liquid effluent containing petroleum fractions from a second cake, said second cake containing said inert solids and being substantially free of hydrocarbon residues.

2. A method in accordance with Claim 1 further comprising the step of adjusting the weight of solids in said waste to about 5 percent or less prior to said heating step.

3. A method in accordance with Claim 1 further comprising the step of passing said aqueous slurry through a screen to remove large particles therefrom prior to said heating step.

4. A method in accordance with Claim 1 further comprising the step of directing said first and second liquid effluents to a refinery.

5. A method in accordance with Claim 1 wherein said second cake contains residual water after being formed in said second centrifugation step, further comprising the step of further dewatering said second cake after said second centrifugation step.

6. A method in accordance with Claim 1 wherein said treating step includes oxidizing polycyclic aromatic hydrocarbons in said second slurry.

7. A method in accordance with Claim 1 wherein said heating step includes injection of steam into said slurry.

8. A method in accordance with Claim 1 wherein at least one of said first and second centrifuges is a disc/bowl centrifuge.

9. A method in accordance with Claim 1 wherein said waste slurry comprises residuals resulting from activities selected from the group consisting of petroleum acquisition, petroleum transporting, petroleum storing, petroleum refining, and combinations thereof, said residuals being selected from the group consisting of sludges, bottoms, waxes, oils, greases, contaminated soils, and mixtures thereof.

10. A method in accordance with Claim 1 wherein said water in said dispersing step is heated.

11. A system for processing oil refinery waste to provide liquid effluent from which petroleum products may be recovered and a cake which is substantially free of hydrocarbon residues, comprising:

a) a conditioning vessel for receiving, tempering, and otherwise thermally conditioning a slurry of said waste;

b) a first centrifuge in communication with said conditioning vessel for receiving said conditioned slurry therefrom and separating said first slurry into a first liquid effluent and a first cake, said first effluent being refinable into petroleum products;

c) a reactor vessel for receiving said first cake;

d) means for dispensing hydrogen peroxide and water into said reactor vessel to form a second slurry with said first cake and to lyse and liberate bound petroleum residues from inert solids contained in said first cake;

e) a second centrifuge in communication with said reactor vessel for receiving said second slurry therefrom and separating said second slurry into a second liquid effluent and a second cake, said second effluent being refinable into petroleum products and said second cake being substantially free of petroleum residues.

12. A system in accordance with Claim 11 wherein at least one of said first and second centrifuges is a disc/bowl centrifuge.

13. A system in accordance with Claim 11 wherein said conditioning vessel is provided with steam for said tempering of said slurry.

14. A system in accordance with Claim 11 further comprising at least one additional reactor vessel arranged for parallel flow with said first reactor vessel.

15. A system in accordance with Claim 11 further comprising means for maintaining non-explosive atmospheres within said conditioning and reactor vessels.

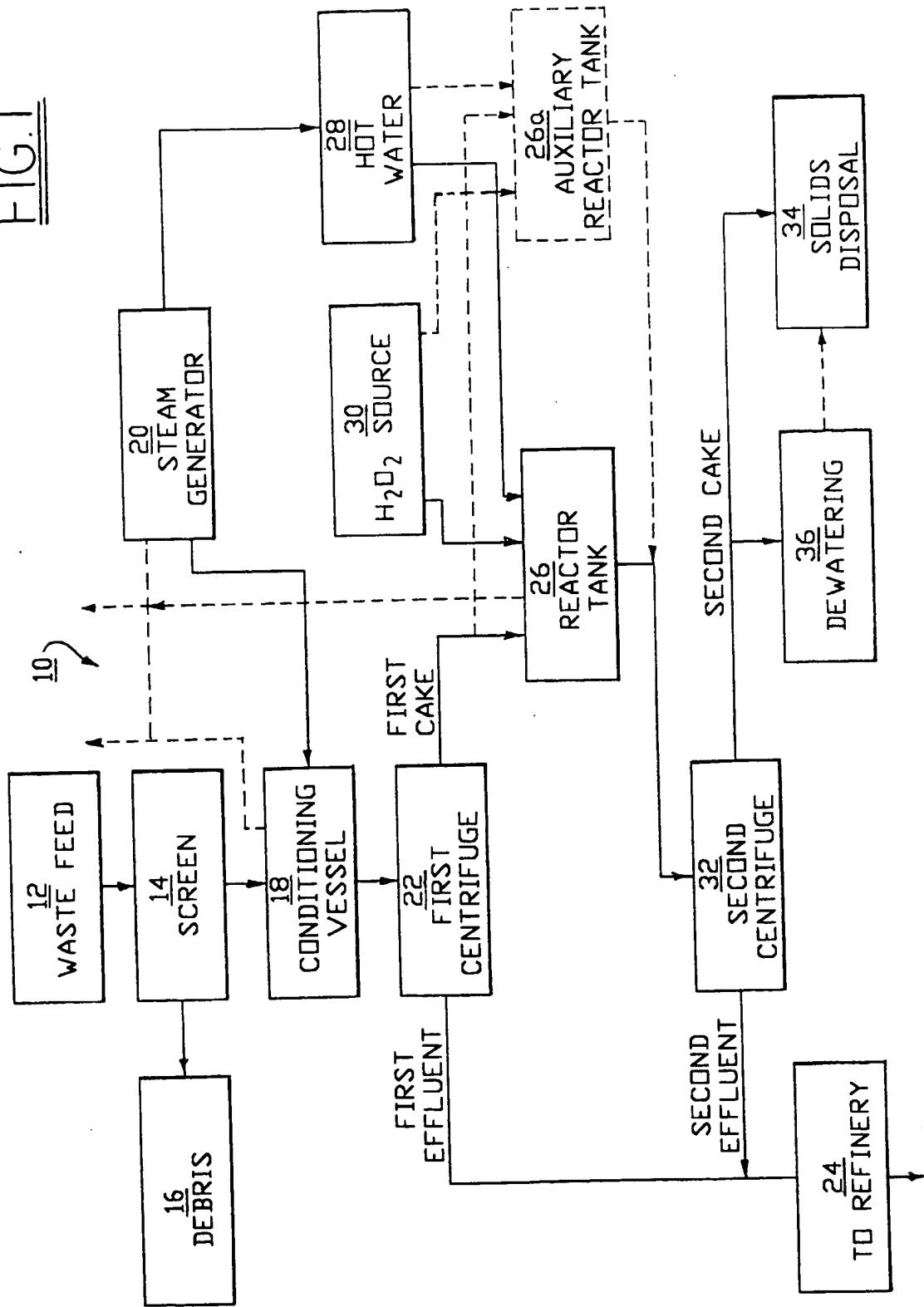
16. A system in accordance with Claim 11 further comprising a screen for filtering large particles from said waste before introducing said waste to said conditioning vessel.

17. A system in accordance with Claim 11 further comprising means for diluting said waste with water to a weight percentage of about 5 percent or less.

18. A system in accordance with Claim 17 further comprising means for capturing volatile hydrocarbons escaping from said slurries and combusting said hydrocarbons to heat said water.

19. A system in accordance with Claim 11 further comprising means for dewatering said second cake.

FIG. 1



INTERNATIONAL SEARCH REPORT

International application No.
PCT/US98/24476

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) :B09C 1/02, 1/08; B01D 21/26

US CL :Please See Extra Sheet.

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 210/759, 766, 768, 771, 772, 774, 787, 806, 175, 177, 198.1, 200, 201, 202, 205, 252, 259, 322, 360.1, 380.1;
405/128, 129

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A,P	US 5,797,701 A (CONAWAY) 25 August 1998 (25-08-98), entire document.	1-19
A	US 5,593,591 A (OHSOL et al.) 14 January 1997 (14-01-97), entire document.	1-19
A	US 5,006,239 A (MISHRA) 09 April 1991 (09-04-91), entire document.	1-19

 Further documents are listed in the continuation of Box C. See patent family annex.

• Special categories of cited documents:	"T"	later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
• "A" document defining the general state of the art which is not considered to be of particular relevance	"X"	document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
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• "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"Z"	document member of the same patent family
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Date of the actual completion of the international search

22 JANUARY 1999

Date of mailing of the international search report

09 FEB 1999

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INTERNATIONAL SEARCH REPORT

International application No.

PCT/US98/24476

A. CLASSIFICATION OF SUBJECT MATTER:

US CL :

210/759, 766, 768, 771, 772, 774, 787, 806, 175, 177, 198.1, 200, 201, 202, 205, 252, 259, 322, 360.1, 380.1;
405/128, 129